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(51) International Patent Classification ⁶ : C08F 10/02	A1	(11) International Publication Number: WO 98/49209 (43) International Publication Date: 5 November 1998 (05.11.98)
(21) International Application Number: PCT/US98/08042 (22) International Filing Date: 21 April 1998 (21.04.98) (30) Priority Data: 08/846,159 25 April 1997 (25.04.97) US (71) Applicant: MOBIL OIL CORPORATION [US/US]; 3225 Gallows Road, Fairfax, VA 22037 (US). (72) Inventors: BARRY, David, Bruce; 2195 Route 27, Edison, NJ 08818 (US). CROTTY, Vincent, Joseph; 3213 Danskin Road, Wall, NJ 07719 (US). EGAN, Brian, John; 231 Maidstone Street, Altona, VIC 3018 (AU). MINK, Robert, Ivan; 30A Gates Avenue, Warren, NJ 07059 (US). NOWLIN, Thomas, Edward; 7 Perrine Path, Cranbury, NJ 08512 (US). SCHREGENBERGER, Sandra, Denise; 5 Hope Court, Ne-shanic, NJ 08853 (US). SCHURZKY, Kenneth, George; 688 North View Drive, Bridgewater, NJ 08807 (US). SHI-RODKAR, Pradeep, Pandurang; 8 McIntire Drive, Belle Mead, NJ 08502 (US). (74) Agents: SCHNELLER, Marina, V. et al.; Mobil Oil Corpora-tion, 3225 Gallows Road, Fairfax, VA 22037 (US).		(81) Designated States: AU, CA, JP, KR, SG, European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). Published <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
(54) Title: PREMIUM PIPE RESINS (57) Abstract The invention relates to the production of high performance conduits. The invention includes the high performance conduits, the polyethylene resin used to make them, and the process for producing the resin which produces a resin with properties which are required, in accordance with the invention to yield the performance characteristics of the resin in conduits. The resin used in accordance with the invention exhibits a bimodal molecular weight distribution or broad molecular weight distribution and is of high molecular weight.		

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PREMIUM PIPE RESINS

The invention relates to premium performance polyethylene conduits, pipe, couplings and liners. High premium performance pipe is useful under conditions which impose high stress and or high service temperatures on the pipe. The
10 conduits may be used for example in pressure or non-pressure applications in mining, gas, waste, and potable water transportation.

The invention relates to the production of high performance conduits. The invention includes the high performance conduits, the polyethylene resin used to make them, and the process for producing the resin with properties which are
15 required to yield the performance characteristics of the subject conduits.

The resin used in accordance with the invention exhibits a bimodal molecular weight distribution or broad molecular weight distribution and is of high molecular weight. It also has a specific distribution of comonomer within the molecular weight distribution. It is produced catalytically in a single reactor.

20 Increasing the molecular weight of polyethylene (and copolymers of ethylene) generally results in enhancing tensile strength, ultimate elongation, impact strength, puncture resistance, and toughness, of films and conduits produced therefrom. However, increasing the molecular weight of the polyethylene will usually decrease its processability. In addition increasing the molecular weight of the molecules that
25 incorporate the comonomer enhances the resistance of polyethylenes to slow crack growth and rupture. By providing a mixture of a high molecular weight polyethylene with a lower molecular weight polyethylene, the desirable characteristics due to the high molecular weight component can be retained while improving processability of the mixture containing the high molecular weight component. Also providing a
30 mixture where the comonomer incorporation is controlled further enhances the performance of these materials. To produce such mixtures, various alternatives have been considered, including post reactor or melt blending, catalysis in a single reactor with a catalyst effective to produce such a product and lastly use of
35 multistage reactors, in which diverse average molecular weight components can be produced in each reactor.

5 The conduits of the invention can be fabricated to diameters in excess of 3 m. The practical lower limit on diameters of conduits that can be manufactured with this invention is 2 to 3 millimeters.

 Wall thickness can range from less than 1 millimeter to in excess of 60 millimeters. The practical range of wall thickness is dependent on the diameter of
10 the conduit being manufactured. This is expressed as a ratio of the wall thickness to diameter, called the Standard Dimension Ratio; SDRs in the range seven to forty can be manufactured from this invention.

 The long term performance of a pipe-grade resin can be evaluated by determining the time-to-failure under constant internal pressure (constant hoop
15 stress), in a controlled environment.

 The conduit of the invention sustains high stresses under conditions of elevated temperature. In accordance herewith, high stress performance is measured by hoop stress tests. Hoop stress measures the pipe burst resistance and the effect of internal pressure and internal pressure build-up on the conduit
20 integrity. It is measured by immersing specimens of pipe in water baths at temperatures from 20° to 80°C, typically 20°, 60° and 80°C. These specimens are then pressured to induce a hoop stress [hoop stress (MPa) = $P (D_m - W_{min}) / 2W_{min}$, where W_{min} is the minimum pipe wall thickness in millimeters, D_m is the mean pipe outside diameter in millimeters, P is the applied pressure in
25 megapascals in the pipe]. Typically in excess of 25 specimens are tested at each test temperature. The time to failure of each specimen is measured. The longer the life at a given hoop stress and temperature the better the performance of the material. This analysis methodology is well documented in International and National Standards, such as ISO 4437, ISO 4427, AS 4131, AS4130, ASTM D 2837,
30 and the standard method for the analysis and prediction of pipe performance as given in ISO/TR 9080 and similar publications.

 Given the long lifetimes required of high performance pipe, hoop stress testing is often conducted at an elevated test temperature, such as 80°C. The time-to-failure under constant internal pressure (constant hoop stress) at 80°C can be
35 used as a measure of performance. At a test temperature of 80°C and a hoop

5 stress of 5.0 MPa, the conduits of the invention exhibit a life-time in excess of 1000 hours, preferably greater than 2500 hours, most preferably greater than 4000 hours.

Resistance to impact failure is an equally important aspect of pipe performance. This was assessed by the Charpy impact test, using an instrumented impactor. Specimen dimensions were 10mm x 30 mm x 160 mm, and the specimens
10 were pre-notched with a notch to width ratio in the range of 0.2 to 0.6. Test temperatures ranged from -60° to +60°C. The span to width ratio of the impactor was 4. The critical strain energy release rate for failure, G_c , was calculated using the principles of linear elastic fracture mechanics. The material characteristic G_c is determined using the specimens described above. The specimen notches vary from
15 3 to 15 millimeters in length, generally notches of 3, 6, 9, 12, and 15 millimeters are used. At a given notch depth at least three samples are tested. The samples are held at the test temperature for two hours prior to testing. Each specimen is then placed in the instrumented impact tester and impacted. The impact tester determines the force displacement curve for the impact. These data are used to
20 determine the energy for fracture, from the area under the force displacement curve. At a given temperature the fracture energies are plotted as a function of the notched specimen dimensions multiplied by a testing geometry factor. This plot is generally linear. The value of G_c for the material, at the temperature of interest, is the slope of the line. (Ref: J. G. Williams, Fracture Mechanics of Polymers, Ellis Horwood,
25 Chichester, 1984.)

Conduits should be resistant to slow crack growth [Refs: ISO 4437, slow crack growth test, and D. Barry and O. Delatycki, J. Polym. Sci., B, Polym. Phys., 25, 883 (1987)]. This property is measured in part by the hoop stress-life time testing cited above; however specific testing is often carried out to determine the
30 resistance to slow crack growth. Resistance to slow crack growth was assessed using the PENT test. This test is described in ASTM 1473-94. Testing is carried out at 80°C, and an initial tensile stress of 2.2 MPa (megapascals). The PENT test measures the time to failure of a 25x10 mm specimen which has a 3 mm sharp notch across one of its broad faces and 1 mm notches across both of its narrow
35 faces. The specimen is tested at a constant load, and this load induces an initial

5 tensile stress of 2.2 MPa in the specimen. Conduits of the invention exhibit PENT
life times in the range of greater than 50 hours preferably greater than 100 hours,
most preferably greater than 150 hours.

The conduits of the invention are produced on conventional pipe extrusion or
pipe winding equipment. One of the advantages of this invention is that conduits
10 with superior performance can be manufactured using conventional equipment.
This is in part due to the ease of processing that the invention imparts due to the
mixture of a low molecular weight and high molecular weight components. The
processability of these materials is assessed using capillary rheometry. A capillary
rheometer measures the apparent viscosity of the material at a given temperature
15 and apparent shear rate. Conduits of the invention, exhibit in the molten state a
lower apparent viscosity at a given apparent shear rate than a conventional
unimodal PE pipe resin of similar melt flow index, FI at 190°C.

The polyethylene resin of the invention is made with a bimetallic catalyst, in a
single reactor, and exhibits a bimodal or broad molecular weight distribution. That is
20 the polyethylene can be characterized as comprising at least two different polymer
components which differ from each other in molecular weight. One of the polymer
components has a higher molecular weight (HMW) compared to the other
component of relatively lower molecular weight (LMW).

The polyethylene resin of the invention, for use in pipe production to make
25 high performance pipe, with the impact resistance, processing advantages,
resistance to slow crack growth, and hoop stress performance characteristics
identified above, must satisfy four physical properties, which relate to density, FI [or
 I_2 , measured accordingly to ASTM D 1238, Condition E], the calculated weight
fraction of the high molecular weight component, and calculated MI of the low
30 molecular weight component. A brief description of the mathematical technique that
is used to estimate the composition (molecular weight and weight fraction) of the
bimodal molecular weight distribution appears in Computer Applications in Applied
Polymer Science, ACS Symposium Series, 197, T. Provder, 45, 1982. The MI of the
low molecular weight component is estimated from a suitable calibration curve
35 based on measured MIs and molecular weights of low molecular weight

5 polyethylenes. In particular, the resins satisfy a density requirement in the range of 0.930 to 0.960 g/cc, preferably 0.935 to 0.955 g/cc, and most preferably 0.940 to 0.950 g/cc. Also, the resins satisfy a FI requirement in the range of 2 to 20 dg/min., preferably 2 to 10 dg/min., most preferably 3 to 8 dg/min. Moreover, the resin must exhibit a weight fraction of the high molecular weight component, based on resin
10 weight, of 0.20 to 0.90, preferably 0.50 to 0.80, most preferably 0.55 to 0.75. In addition, the low molecular weight component must exhibit a calculated MI of 200 to 10000 dg/min., preferably 200 to 5000 dg/min., most preferably 200 to 3000 dg/min.

The resin of this invention may be either 1) a homopolymer of ethylene; 2) at least one copolymer of a preponderance i.e., greater than 50 wt.% of ethylene with a
15 minor amount of a 1-olefin containing 3 to 10 carbon atoms, preferably a 1-olefin containing 4 to 10 carbon atoms, e.g., 1-butene, 1-pentene, 1-hexene, 4-methyl-1-pentene, 1-octene, 1-decene, and mixtures thereof; or 3) a mixture of any of the foregoing polymers. In general, the polymer product will comprise an amount of polymerized comonomer which is in the range, for example, of 0 to 30 wt.%, based
20 on the total weight of polymer.

The resins of the invention comprise a HMW component and a LMW component with a HMW component weight fraction which is greater than 0 (zero). The resin has a molecular weight distribution, which is characterized as MFR or M_w/M_n . The MFR of resin products of the invention can range from 20 to 300,
25 preferably from 40 to 200, and most preferably from 50 to 150. The M_w/M_n of resin products of the invention can range from 2.5 to 60, preferably from 5 to 40, and most preferably from 10 to 30.

The compositions of the invention can be extruded into pipes and injection or blow molded into articles or extruded and blown into films. Films can be produced
30 which are 0.2 to 10.0 mils, preferably 0.5 to 2.0 mils, thickness. Blow molded articles include bottles, containers, fuel tanks and drums.

The polyethylene resins of the invention need not be blended with other polyolefins, e.g., polyethylenes and ethylene copolymers. However, it is contemplated that the resins may be blended with other polyolefins and copolymers
35 of e.g., ethylene such as LLPPE. Thus, the invention contemplates a composition

- 5 for pipe production comprising greater than 80% by weight of the bimodal or broad molecular weight distribution polyethylene resin.

The products may contain any of various additives conventionally added to polymer compositions such as lubricants, stabilizer, antioxidants, compatibilizers and pigments. These reagents can be employed to stabilize the products against
 10 degradation. For example, additive packages comprising 400-2000 ppmw hindered phenol(s); 200-2000 ppmw phosphites; 250-3000 ppmw stearates, and 0.5 to 3.0 wt.% carbon black, for addition to the resin powders, can be used for pelletization.

The following Examples further illustrate the essential features of the invention. However, it will be apparent to those skilled in the art that the specific
 15 reactants and reaction conditions used in the Examples do not limit the scope of the invention.

The properties of the polymers produced in the Examples were determined by the following test methods:

20	Density	ASTM D 1505 - a plaque is made and conditioned for one hour at 100°C to approach equilibrium crystallinity. Measurement for density is then made in a density gradient column; reported as gms/cc.
25	Melt Index (MI), I_2	ASTM D 1238 - (190°C/2160 g) Measured at 190°C - reported as grams per 10 minutes.
30	High Load Melt Index (HLMI), $I_{21.6}$ or FI	ASTM D 1238 - (190°C/21600 g) Measured at 10 times the weight used in the melt index test above.
35	Melt Flow Ratio I_{21}/I_2	It is noted that $I_{21.6}$ and I_{21} are used interchangeably herein.

When the resin is made with the preferred catalyst described below it will contain 0.5 to 20 ppm of transition metals. In particularly preferred embodiments
 40 described herein, the resin will contain 0.1 to 10 ppm Zr and 0.5 to 10 ppm Ti. The

- 5 as formed reactor product is granular and has a preferred average particle size range of 0.01 - .04 inches.

The result of the process conducted in the fluidized bed gas phase reactor is a particulate resin product. Particles of this resin exhibit very uniform molecular weight and molecular weight distribution. This uniformity is attributable to a catalyst
10 which contains the two transition metals. Production of bimodal molecular weight or broad molecular weight distribution resins by altering process conditions in two reactors in series does not allow for this uniformity. In a preferred embodiment, the invention relates to the production of titanium/zirconium-based bimetallic catalyst systems that produce broad and/or bimodal MWD polyethylene resins in a single
15 reactor. In the most preferred embodiment, the LMW component in the resin is produced by the Zr active centers, while the HMW component is produced by the Ti active centers. The relative productivity of the two active centers determines the ratio of the HMW and the LMW components in the final resin.

The Catalyst

20 In accordance with the invention, these catalysts are made by a process for forming a carrier material impregnated with alumoxane and derivatives thereof comprising the steps:

(1) providing silica which is porous and has a particle size of 1 to 250 microns, having pores which have an average diameter of 50 to 500 Angstroms and
25 having a pore volume of 0.5 to 5.0 cc/g;

(2) slurring the silica in an aliphatic medium;

(3) providing a volume of a solution comprising a metallocene, alumoxane of formulas $R-(Al(R)-O)_x-AlR_2$ for oligomeric linear alumoxanes and $(-Al(R)-O)_y$ for cyclic alumoxanes wherein x is 1-40, y is 3-40, and R is a C₁-C₈ alkyl group in an
30 aromatic solvent, wherein the concentration of alumoxane, expressed as Al wt.% is 1 to 20; and wherein the volume of the solution is sufficient to impregnate the pores of silica without forming a slurry of the silica in the aromatic solvent;

(4) contacting the silica with said volume of said solution (3); and

- 5 (5) evaporating liquid phase from the impregnated silica to recover dry free-flowing catalyst particles.

The metallocene complex becomes more uniformly distributed throughout the support as a result of steps (2) and (4). When two transition metal sources exhibiting different hydrogen responses in ethylene polymerization reactions are
10 supported on the carrier subjected to the process of the invention, the result of the catalyst preparation process is an olefin polymerization catalyst composition which produces less gels in the polyethylene film produced from the polyethylene prepared with the catalyst composition. In the process of the invention, step (2) may be undertaken prior to or after step (4).

- 15 The carrier material is a solid, particulate, porous, preferably inorganic material, such as an oxide of silicon and/or of aluminum. The carrier material is used in the form of a dry powder having an average particle size of from 1 micron to 500 microns, preferably from 10 microns to 250 microns. The surface area of the carrier is at least 3 square meters per gram (m^2/g), and preferably at least 50 m^2/g
20 up to 350 m^2/g . The carrier material should be free of absorbed water. Drying of the carrier material can be effected by heating at 100°C to 1000°C, preferably at 600° C. When the carrier is silica, it is heated to at least 200° C, preferably 200°C to 850°C and most preferably at 600 °C. The carrier material must have at least some active hydroxyl (OH) groups to produce the catalyst composition of this
25 invention.

- In the most preferred embodiment, the carrier is silica which, prior to the use thereof in the first catalyst synthesis step, has been dehydrated by fluidizing it with nitrogen and heating at 600°C for 4-16 hours to achieve a surface hydroxyl group concentration of 0.7 mmol/g. The silica of the most preferred embodiment is a high
30 surface area, amorphous silica (surface area = 300 m^2/g ; pore volume of 1.65 cm^3/g), and it is a material marketed under the tradenames of Davison 952 or Davison 955 by the Davison Chemical Division of W.R. Grace and Company or Crosfield ES70 by Crosfield Limited. The silica is in the form of spherical particles

- 5 and obtained by the spray-drying process. As procured, these silicas are not calcined and this must be dehydrated, as indicated above.

The catalyst synthesis is undertaken under inert conditions in the absence of water and oxygen.

- The carrier material having said OH groups is slurried in a non-polar solvent.
- 10 The slurry of the carrier material is prepared by introducing the carrier into the solvent, preferably while stirring, and heating the mixture to 25° to 70°C, preferably to 40° to 60°C. Temperature of the slurry is critical with respect to the activity of the catalyst components added to it. All catalyst precursor synthesis steps should be conducted at temperatures below 90°C.

- 15 In embodiments of the invention, incorporation of the first transition metal component in the catalyst occurs prior to undertaking steps (3) and (4). In specific embodiments, incorporation of the first transition metal component involves a series of steps. Initially, the carrier is contacted with an organomagnesium compound which has the empirical formula $R_mMgR'_n$ where R and R' are the same or different
- 20 C_2 - C_{12} alkyl groups, preferably C_4 - C_{10} alkyl groups, more preferably C_4 - C_8 alkyl groups, and most preferably both R and R' are butyl groups, and m and n are each 0, 1 or 2, providing that $m + n$ is equal to the valence of Mg. Optionally, but preferably, the organomagnesium-impregnated carrier is thereafter contacted with an alcohol and lastly with a non-metallocene transition metal source. Most
- 25 preferably, these steps are undertaken in the order noted and without isolation of a dry product until after the non-metallocene transition metal compound incorporation.

- Suitable non-polar solvents for slurrying silica and introduction of the first transition metal component are materials which are liquid at reaction temperatures and in which all of the reactants used herein, i.e., the organomagnesium compound,
- 30 the alcohol and the transition metal compound, are at least partially soluble. Preferred non-polar solvents are alkanes, such as isopentane, hexane, isohexane, n-heptane, octane, nonane, and decane, although a variety of other materials including cycloalkanes, such as cyclohexane, aromatics, such as benzene, toluene and ethylbenzene, may also be employed. The most preferred non-polar solvents

5 are isopentane and isohexane. Prior to use, the non-polar solvent should be purified, such as by percolation through silica gel and/or molecular sieves, to remove traces of water, oxygen, polar compounds, and other materials capable of adversely affecting catalyst activity. In certain embodiments of the invention, two aliphatic solvents may be used, one for the incorporation of the non-metallocene
10 transition metal compound and second aliphatic solvent for use in the incorporation of the metallocene transition metal compound dissolved in an aromatic solvent. Accordingly, in the embodiment of titanium incorporation into the silica with the aliphatic solvent, that solvent will be referred as the first aliphatic solvent; and when an aliphatic solvent is used in conjunction with metallocene compound incorporation
15 into the support, that aliphatic solvent will be referred as the second aliphatic solvent.

In the most preferred embodiment of the synthesis of this catalyst it is important to add only such an amount of the organomagnesium compound to the silica slurry that will be deposited, physically or chemically, into the support since
20 any excess of the organomagnesium compound in the solution may react with the other synthesis chemicals and precipitate outside of the support. The carrier drying temperature affects the number of sites on the carrier available for the organomagnesium compound: the higher the drying temperature the lower the number of sites. Thus, the exact molar ratio of the organomagnesium compound to
25 the hydroxyl groups will vary and must be determined on a case-by-case basis to assure that only so much of the organomagnesium compound is added to the solution as will be deposited into the support without leaving any excess of the organomagnesium compound in the solution. Thus, the molar ratios given below are intended only as an approximate guideline and the exact amount of the
30 organomagnesium compound in this embodiment must be controlled by the functional limitation discussed above, i.e., it must not be greater than that which can be deposited into the support. The required amount of the organomagnesium compound can be determined in any conventional manner, e.g., by adding the organomagnesium compound to the slurry of the carrier in the solvent, while stirring
35 the slurry, until the organomagnesium compound is detected in the liquid phase.

5 For example, for the silica carrier heated at 600°C, the amount of the organomagnesium compound added to the slurry is such that the molar ratio of Mg to the hydroxyl groups (OH) on the solid carrier is 0.5:1 to 4:1, preferably 0.8:1 to 3:1, more preferably 0.9:1 to 2:1 and most preferably 1:1. The organomagnesium compound dissolves in the non-polar solvent to form a solution from which the
10 organomagnesium compound is deposited into the carrier. The amount of the organomagnesium compound based on the amount of silica ranges from 0.2 mmol/g to 2 mmol/g, preferably from 0.4 mmol/g to 1.5 mmol/g, more preferably from 0.6 mmol/g to 1.0 mmol/g, and most preferably from 0.7 mmol/g to 0.9 mmol/g.

It is also possible to add the organomagnesium compound in excess of the
15 amount deposited into the support and then remove it, e.g., by filtration and washing. However, this alternative is less desirable than the most preferred embodiment described above.

The organomagnesium compound-treated support is contacted with an organic alcohol (ROH) containing RO groups which displace alkyl groups attached
20 to the magnesium atom. The amount of the alcohol is effective to provide a ROH:Mg [mol/mol] ratio which ranges from 0.2 to 1.5, preferably from 0.4 to 1.2, more preferably from 0.6 to 1.1, most preferably from 0.9 to 1.0.

Contact of the silica-supported magnesium compound with the alcohol is also undertaken in the slurry at a temperature ranging from 25° to 80°C, preferably at 40°
25 to 70°C.

The alkyl group in the alcohol can contain 1 to 12 carbon atoms, preferably 1 to 8; in the embodiments below, it is an alkyl group containing 2 to 4 carbon atoms, particularly four carbon atoms (n-butanol). The inclusion of the alcohol addition step in the catalyst synthesis of the invention produces a final catalyst which is much
30 more active, requires much less non-metallocene transition metal compound (e.g., or titanium compound) and is much more active with respect to the metallocene complex, as opposed to exclusion of the alcohol addition step.

After the addition of the alcohol to the slurry is completed, the slurry is contacted with the first source of transition metal compound, a preferably non-
35 metallocene transition metal compound. The slurry temperature at this stage must

5 be maintained at 25° to 70°C, preferably to 40° to 60°C, because temperatures above 80°C can result in deactivation of the non-metallocene transition metal component. Suitable non-metallocene transition metal compounds used herein are compounds of metals of Groups 4A, and 5A, of the Periodic Chart of the Elements, as published by Chemical and Engineering News, 63(5), 27, 1985, providing that
10 such compounds are soluble in the non-polar solvents. Non-limiting examples of such compounds are titanium and vanadium halides, e.g., titanium tetrachloride, vanadium tetrachloride, vanadium oxytrichloride, titanium and vanadium alkoxides, wherein the alkoxide moiety has a branched or unbranched alkyl radical of 1 to 20 carbon atoms, preferably 1 to 6 carbon atoms. The preferred transition metal
15 compounds are titanium compounds, preferably tetravalent titanium compounds. The most preferred titanium compound is TiCl_4 . The amount of titanium or vanadium ranges from a Ti/Mg molar ratio of 0.1 to 2.0, preferably from 0.3 to 1.0.

Mixtures of such transition metal compounds may also be used and generally no restrictions are imposed on the transition metal compounds which may be
20 included. Any transition metal compound that may be used alone may also be used in conjunction with other transition metal compounds. After the addition of the first transition metal compound is completed, the solvent is removed by evaporation or filtering to obtain a free-flowing powder of the catalyst intermediate. Next, incorporation of the metallocene transition metal compound into the catalyst
25 intermediate is undertaken. The metallocene compound is pre-activated with an alkyl alumoxane.

Incorporation of the metallocene complex and its uniform distribution in the support is achieved in a mixed solvent system.

The metallocene compound has the formula $\text{Cp}_x\text{MA}_y\text{B}_z$ in which Cp is an
30 unsubstituted or substituted cyclopentadienyl group, M is zirconium or hafnium atom and A and B belong to the group including a halogen atom, hydrogen atom or an alkyl group. In the above formula of the metallocene compound the preferred transition metal atom M is zirconium. In the above formula of the metallocene compound, the Cp group is an unsubstituted, a mono- or a polysubstituted

5 cyclopentadienyl group; and x is at least 1. The substituents on the cyclopentadienyl group can be preferably straight-chain C₁-C₆ alkyl groups. The cyclopentadienyl group can be also a part of a bicyclic or a tricyclic moiety such as indenyl, tetrahydroindenyl, fluorenyl or a partially hydrogenated fluorenyl group, as well as a part of a substituted bicyclic or tricyclic moiety. In the case when x in the
 10 above formula of the metallocene compound is equal to 2, the cyclopentadienyl groups can be also bridged by polymethylene or dialkylsilyl groups, such as -CH₂-, -CH₂-CH₂-, -CR'R"- and -CR'R"-CR'R"- where R' and R" are short alkyl groups or hydrogen atoms, -Si(CH₃)₂-, Si(CH₃)₂-CH₂-CH₂-Si(CH₃)₂- and similar bridge groups. If the A and B substituents in the above formula of the metallocene
 15 compound are halogen atoms, they belong to the group of fluorine, chlorine, bromine or iodine; and y + z is 3 or less, provided that x + y + z equals the valence of M. If the substituents A and B in the above formula of the metallocene compound are alkyl groups, they are preferably straight-chain or branched C₁-C₈ alkyl groups, such as methyl, ethyl, n-propyl, isopropyl, n-butyl, isobutyl, n-pentyl, n-hexyl or n-
 20 octyl.

Suitable metallocene compounds include bis(cyclopentadienyl)metal dihalides, bis(cyclopentadienyl)metal hydridohalides, bis(cyclopentadienyl)metal monoalkyl monohalides, bis(cyclopentadienyl)metal dialkyls and bis(indenyl)metal dihalides wherein the metal is a zirconium or hafnium atom, halide groups are
 25 preferably chlorine atoms and the alkyl groups are C₁-C₆ alkyls. Illustrative, but non-limiting examples of metallocenes include

Bis(indenyl)zirconium dichloride,
 Bis(indenyl)zirconium dibromide,
 Bis(indenyl)zirconium bis(p-toluenesulfonate),
 30 Bis(4,5,6,7-tetrahydroindenyl)zirconium dichloride,
 Bis(fluorenyl)zirconium dichloride,
 Ethylenebis(indenyl)zirconium dichloride,
 Ethylenebis(indenyl)zirconium dibromide,
 Ethylenebis(indenyl)dimethylzirconium,

- 5 Ethylenebis(indenyl)diphenylzirconium,
Ethylenebis(indenyl)methylzirconium chloride,
Ethylenebis(indenyl)zirconium bis(methanesulfonate),
Ethylenebis(indenyl)zirconium bis(ptoluenesulfonate),
Ethylenebis(indenyl)zirconium bis(trifluoromethanesulfonate),
10 Ethylenebis(4,5,6,7 tetrahydroindenyl)zirconium dichloride,
Isopropylidene(cyclopentadienyl)(fluorenyl)zirconium dichloride,
Isopropylidene(cyclopentadienyl)(methylcyclopentadienyl) zirconium
dichloride,
Dimethylsilylbis(cyclopentadienyl)zirconium dichloride,
15 Dimethylsilylbis(methylcyclopentadienyl)zirconium dichloride,
Dimethylsilylbis(dimethylcyclopentadienyl)zirconium dichloride,
Dimethylsilylbis(trimethylcyclopentadienyl)zirconium dichloride,
Dimethylsilylbis(indenyl)zirconium dichloride,
Dimethylsilylbis(indenyl)zirconium bis(trifluoromethanesulfonate),
20 Dimethylsilylbis(4,5,6,7-tetrahydroindenyl)zirconium dichloride,
Dimethylsilyl(cyclopentadienyl)(fluorenyl)zirconium dichloride,
Diphenylsilylbis(indenyl)zirconium dichloride,
Methylphenylsilylbis(indenyl)zirconium dichloride,
Bis(cyclopentadienyl)zirconium dichloride,
25 Bis(cyclopentadienyl)zirconium dibromide,
Bis(cyclopentadienyl)methylzirconium chloride,
Bis(cyclopentadienyl)ethylzirconium chloride,
Bis(cyclopentadienyl)cyclohexylzirconium chloride,
Bis(cyclopentadienyl)phenylzirconium chloride,
30 Bis(cyclopentadienyl)benzylzirconium chloride,
Bis(cyclopentadienyl)zirconium chloride monohydride,
Bis(cyclopentadienyl)hafnium monochloride monohydride,
Bis(cyclopentadienyl)methylzirconium hydride,
Bis(cyclopentadienyl)dimethylzirconium,
35 Bis(cyclopentadienyl)dimethylhafnium,

- 5 Bis(cyclopentadienyl)diphenylzirconium,
 Bis(cyclopentadienyl)dibenzylzirconium,
 Bis(cyclopentadienyl)methoxyzirconium chloride
 Bis(cyclopentadienyl)ethoxyzirconium chloride,
 Bis(cyclopentadienyl)zirconium bis(methanesulfonate),
10 Bis(cyclopentadienyl)zirconium bis(p-toluenesulfonate),
 Bis(cyclopentadienyl)zirconium bis(trifluoromethanesulfonate),
 Bis(methylcyclopentadienyl)zirconium dichloride,
 Bis(dimethylcyclopentadienyl)zirconium dichloride,
 Bis(dimethylcyclopentadienyl)ethoxyzirconium chloride,
15 Bis(dimethylcyclopentadienyl)zirconium bis(trifluoromethanesulfonate),
 Bis(ethylcyclopentadienyl)zirconium dichloride,
 Bis(methylethylcyclopentadienyl)zirconium dichloride,
 Bis(propylcyclopentadienyl)zirconium dichloride,
 Bis(methylpropylcyclopentadienyl)zirconium dichloride,
20 Bis(butylcyclopentadienyl)zirconium dichloride,
 Bis(butylcyclopentadienyl)hafnium dichloride
 Bis(methylbutylcyclopentadienyl)zirconium dichloride,
 Bis(methylbutylcyclopentadienyl)zirconium bis(methanesulfonate),
 Bis(trimethylcyclopentadienyl)zirconium dichloride,
25 Bis(tetramethylcyclopentadienyl)zirconium dichloride,
 Bis(pentamethylcyclopentadienyl)zirconium dichloride,
 Bis (pentamethylcyclopentadienyl)zirconium dichloride,
 Bis(hexylcyclopentadienyl)zirconium dichloride,
 Bis(trimethylsilylcyclopentadienyl)zirconium dichloride,
30 Bis(n-butylcyclopentadienyl)hafnium monochloride monohydride,
 Bis (n-butylcyclopentadienyl)zirconium monochloride monohydride.

The metallocene compounds utilized within the embodiment of this art can be used as crystalline solids or solutions in hydrocarbons.

5 Alumoxanes activate metallocene transition metal compounds. The class of alumoxanes comprises oligomeric linear and/or cyclic alkylalumoxanes represented by the formula:

$R-(Al(R)-O)_n-AlR_2$ for oligomeric linear alumoxanes and

$(-Al(R)-O-)_m$ for oligomeric cyclic alumoxanes

10 wherein n is 1-40, preferably 10-20, m is 3-40, preferably 3-20 and R is a C_1-C_8 alkyl group, preferably methyl group. MAO (methylalumoxane) is a mixture of oligomers with a very wide distribution of molecular weights and usually with an average molecular weight of 1200. MAO is typically kept in solution in toluene. In one embodiment, the amount of Al, provided by alumoxane, is sufficient to provide
15 an Al:transition metal (provided by metallocene) molar ratio ranging from 50 to 500, preferably 75 to 300, more preferably from 85 to 200, and most preferably from 90 to 150.

In accordance with the invention, deposition of the metallocene complex admixed with alumoxane into the carrier is undertaken using the free-flowing powder
20 containing a non-metallocene transition metal compound impregnated into the carrier. The free-flowing powder is pre-slurried in a light aliphatic solvent. The pore volume of the carrier is determined and metallocene-alumoxane solution is provided in a volume equal to or less than two times the total pore volume of the carrier.

The volume of the solution comprising the alumoxane, the metallocene
25 complex and the aromatic solvent therefore can vary. In the preferred embodiment, the volume of the solution comprising the solvent and metallocene-alumoxane ingredients is lower than that necessary to form a slurry of the carrier material, such as silica, but sufficient to fill the pores of the carrier material. Accordingly and preferably, the maximum volume of the alumoxane-metallocene solution does not
30 exceed two times the total pore volume of the carrier material. Accordingly, if the pore volume of the carrier material is $1.65\text{cm}^3/\text{g}$, then the volume of alumoxane-metallocene solution will be equal to or less than $3.30\text{cm}^3/\text{gram}$ of carrier material.

The solvent used to form this solution is one in which each of the metallocene, alumoxane, and activated mixtures thereof are soluble. Preferably,

- 5 this solvent is an aromatic solvent selected from the group consisting of benzene, xylene or toluene. The most preferred solvent is toluene.

As indicated above, incorporation and uniform dispersion of the metallocene complex in the carrier involves a system consisting of at least two solvents. In accordance with the invention, the first solvent used during the addition of RMgR' ,
10 ROH and TiX_4 to silica, to form a Ziegler type catalyst intermediate is preferably aliphatic; it may consist of straight or branched chain hydrocarbons with 4 to 7 carbon atoms. Examples include isobutane, pentane, isopentane, hexane, isohexanes, heptane, isoheptanes.

The second aliphatic solvent is used to slurry the catalyst intermediate and to
15 receive or to disperse the solution containing the source of metallocene compound in an aromatic solvent.

The liquid medium in the final step of catalyst preparation comprises a volume ratio of the aliphatic solvent to the aromatic solvent which ranges from 0.5 to 30. The slurry is agitated to insure good mixing while the solution of metallocene
20 compound and alumoxane is added to the slurry of the carrier material.

The liquid phase is evaporated from the slurry to isolate a free-flowing powder containing two sources of transition metal without any filtering. Filtering is avoided to substantially eliminate the loss of catalytic components. The liquid phase is removed by evaporation at relatively low temperatures, in the range above
25 40°C and below 50°C . Very short heating time schedules are employed to obviate catalyst degradation.

In a preferred embodiment, the metallocene is added to the solution of the alumoxane prior to impregnating the carrier with the solution. Again, as noted above, the maximum volume of the alumoxane solution also including the
30 metallocene compound should not exceed two times the total pore volume of the carrier material. The molar ratio of alumoxane, expressed as Al, to metallocene metal expressed as M (e.g. Zr), ranges from 50 to 500, preferably 75 to 300, and most preferably 90 to 150. An added advantage of the present invention is that this Al:Zr ratio can be directly controlled. In a preferred embodiment the alumoxane and

5 metallocene compound are mixed together at a temperature of 20° to 80°C, for 0.1 to 24 hours, prior to use in the deposition step. The solvent for the metallocene compound and alumoxane can be hydrocarbons or halogenated aromatic hydrocarbons, preferably it is toluene.

The catalyst precursor component formed from the organomagnesium
10 compound, the non-metallocene transition metal compound and the activated metallocene complex, must be activated with a cocatalyst, which is an alkylaluminum compound. Preferably, trimethylaluminum (TMA) is the cocatalyst. The amount of TMA is sufficient to give an Al:Ti molar ratio of 1:1 to 1000:1, preferably 5:1 to 300:1, and most preferably 5:1 to 100:1. The activated catalyst
15 composition exhibits high activity for long periods of time and shows little deactivation.

Olefins are polymerized with catalysts according to the present invention by any suitable process. Such processes include polymerization carried out in suspension, in solution or in the gas phase. Gas phase polymerization reactions
20 are preferred, e.g., those taking place in stirred bed reactors and, especially, fluidized bed reactors. The polymerization is carried out at relatively low temperatures, e.g. from 30° to 115°C. Preferably, polymerization pressures are less than 10,000 psi, preferably less than 1000 psi, and most preferably in the range of 100 to 350 psi.

25 A particularly desirable method for producing polyethylene polymers according to the present invention is in a fluid-bed reactor. Such a reactor and means for operating it are described by Nowlin et al. in U.S. Patent No. 4,481,301. The polymer produced in such a reactor contains the catalyst particles because the catalyst is not separated from the polymer. The molecular weight of the polymer
30 may be controlled in a known manner, e.g., by using hydrogen. With the catalysts produced according to the present invention, molecular weight may be suitably controlled with hydrogen when the polymerization is carried out at relatively low temperatures, e.g., from 30° to 105°C. This control of molecular weight may be evidenced by a measurable positive change in melt index (I_2) of the polymer
35 produced.

5 When a fluid-bed reactor is employed, the catalyst modifier of the invention can be introduced separately. The catalyst modifier is water. The amount of the catalyst modifier can range from 0.1 to 1000 ppm (based on ethylene), and preferably from 0.1 to 50 ppm (based on ethylene). The water cofeed can range from 0.1 ppm to 1000 ppm based on ethylene; generally 0.1 to 50 ppm water, based
10 on ethylene, is employed. Although the catalyst modifier can be added separately, it can also be added as a mixture, a cofeed, with ethylene or hydrogen.

EXAMPLES

Example 1: U.S. Patent Appln. No. 08/555816 filed November 9, 1995 describe procedures for producing the catalyst used to make the resin of the invention.

15 Titanium component: Into a 200 gallon mix vessel containing a helical stirrer was added Davison-grade 955 silica (61.0 lb), which was previously calcined at 600°C for 4 h, and isopentane (138 liter). The agitator speed was set at 100 rpm and the internal temperature of the vessel was set at 50° to 55°C. Dibutylmagnesium solution in heptane (19.90 mol) was added to the stirred silica/isopentane slurry and
20 stirring was continued for one hour. 1-Butanol (18.91 mol) was added to the slurry and stirring was continued for 1 h. Then, TiCl_4 (11.94 mol) was added to the reaction medium and stirring was continued for 1 h. Then the agitator speed was reduced to 40 rpm and the liquid phase was removed by evaporation under a nitrogen purge to provide a free-flowing light tan powder. Elemental analyses: Ti,
25 1.66 wt.%; Mg, 1.36 wt. %.

Bimetallic Catalyst: The dry titanium component from above (393.5g) was placed into a 2-gallon glass vessel containing a helical stirrer which was set at 150 rpm. About 1970 ml of isopentane was added to the glass vessel. Then, at ambient temperature was added a toluene solution (629 ml) containing MAO (7.00 mmol Al/g
30 titanium component) and $(n\text{-BuCp})_2\text{ZrCl}_2$ (7.42g) over a period of 15 minutes. After one hour, the internal temperature was increased to 45°C and the liquid phase was removed under a nitrogen purge for 5 h to provide a brown free-flowing powder. Elemental analyses: Ti, 1.02 wt%; Zr, 0.27 wt%. The catalyst for run #6 in the

- 5 Table was prepared in the foregoing synthesis. The other catalysts were prepared by similar synthesis but for variation in the loading and Al:Zr ratio.

Example 2: We produced a series of resins in a gas phase reactor using catalysts that were prepared as described in Example 1. The process conditions, resin characteristics, catalyst composition and the pipe performance are tabulated in the
10 attached table. For comparison we have also included pipe resins available commercially from Kemcor Australia Proprietary Limited (HD2468 and MD0898). The invention pipe resins provide superior performance as indicated by longer failure times and higher impact strength.

Extended hoop stress testing of sample 1 from Example 2 has been
15 conducted at 20°, 60° and 80°C. The data was analyzed according to ISO TR 9080. This analysis indicated that Example 2, sample 1, would sustain a design hoop stress, σ_{td} , of 6.1 MPa at 50°C for 50 years. This compares to performances of 1 year at 6.7 MPa for HD2468 and 28 years at 6.7 for MD0898, both at 50°C.

	1	2	3	4	5	6	7	8	9	HD2468 (Kemcor)	MD0898 (Kemcor)
RESIN PROPERTIES											
FI (dg/min)	4.6	5.4	3.9	4.2	4.9	3.5	7.2	5.6	6.5	14	13
Density (g/cc)	0.946	0.947	0.946	0.944	0.944	0.946	0.947	0.949	0.952	0.947	0.942
Xhmw	0.64	0.64	0.69	0.72	0.67	0.67	0.61	0.63	0.65	N/A	N/A
Mllmw (dg/min)	1050	1700	2450	1750	1850	1000	1250	2550	1750	N/A	N/A
Zr residue (ppm)	*	1.06	1.16	1.09	.91	1.41	1.63	*	1.16	N/A	N/A
PIPE PROPERTIES											
Time-to-fail (hrs)	1650	2835	>4075	>5280	>1300	3595	3080	840	235	400	600
Impact, G _c (kJ/m ²)	17	*	*	*	*	*	*	16	*	6	5
REACTOR CONDITIONS											
Reactor T (C)	95	95	95	95	95	90	98	90	94		
Ethylene PP (PSI)	173	184	182	174	174	183	190	188	171		
Isopentane PP (PSI)	34	33	33	34	2	41	24	32	37		
C ₆ C ₂ Feed Wt. Ratio	0.025	0.032	0.031	0.037	0.032	0.025	0.030	~0.018	0.014		
H ₂ :C ₂ Molar Ratio	0.010	0.0074	0.0080	0.0107	0.0075	0.0103	0.0070	0.0095	0.0096		
TMA feed (ppmw)	126	90	98	127	127	129	173	~123	124		
Water Feed (ppmv)	63	19.7	19.3	9.1	14.2	0	2.1	~3	18.3		
CATALYST COMPOSITION											
Al:Zr molar ratio	100	120	120	120	120	150	100	100	120		
MAO loading (mmol Al from MAO/g Ti component)	6	6	6	6	6.8	7	6	6	6.8		

(* indicates property not measured for this sample)

5 CLAIMS:

1. A conduit comprising a polyethylene resin selected from the group consisting of polymers and copolymers of ethylene and admixtures thereof, wherein
10 the resin is characterized by FI $\{I_{21.6}$, measured according to ASTM D 1238, Condition F} of 2 to 20 dg/min and wherein the resin is made with a catalyst comprising a metallocene transition metal compound wherein the resin contains a catalyst residue and thus contains up to 20 ppm of transition metal provided by said metallocene transition metal compound.
15
2. The conduit of Claim 1, wherein the resin contains 0.1 to 10 ppm zirconium.
3. The conduit of Claim 1, which is characterized by a life time of at least
20 100 hours at a hoop stress of 5 megapascal (MPa) at 80°C and an impact strength of greater than 3 kJ/m² at 0°C.
4. The conduit of Claim 3, wherein said life time is greater than 500
hours.
25
5. The conduit of Claim 3, wherein said life time is greater than 1000 hours.
6. The conduit of Claim 3, wherein said impact strength is greater than 5
30 kJ/m² at 0°C.
7. The conduit of Claim 3, wherein said impact strength is greater than 10 kJ/m² at 0°C.

5 8. The conduit of Claim 1 wherein the resin exhibits a density of 0.930 to
0.96 g/cc.

 9. The conduit of Claim 1, which comprises greater than 80% by weight
of said polyethylene resin.

10

 10. The conduit of Claim 1, wherein the resin is produced in one reactor, is
characterized as comprising at least two components which differ from each other in
average molecular weight, one component of said at least two components
exhibiting a higher average molecular weight than a second of said two components
15 which second component exhibits a lower average molecular weight than said one
component.

 11. The conduit of Claim 10, wherein said second component exhibits a
calculated MI [_{12.16} according to ASTM D 1238, Condition E] of 200 to 10,000dg./min.

20

 12. The conduit of Claim 1, which is characterized by a time to failure
when PENT tested, in accordance with ASTM 1473-94, at 80°C and an initial tensile
stress of 2.2 MPa, of greater than 50 hours.

25 13. The conduit of Claim 10, wherein said one component is present in the
resin as a calculated weight fraction in the range of 0.20 to 0.90

 14. The conduit of Claim 10, wherein said one component is present in
the resin as a calculated weight fraction in the range of 0.50 to 0.80

30

 15. The conduit of Claim 10, wherein said one component is present in the
resin as a calculated weight fraction in the range of 0.55 to 0.75

5 16. The conduit of Claim 10, wherein the resin exhibits a density of 0.930 to 0.96 g/cc.

 17. The conduit of Claim 16, wherein the resin exhibits a density of 0.935 to 0.955 g/cc.

10

 18. The conduit of Claim 17, wherein the resin exhibits a density of 0.940 to 0.950 g/cc.

 19. The conduit of Claim 5, wherein the resin is produced in one reactor, is
15 characterized as comprising at least two components which differ from each other in average molecular weight, one component of at least two said components exhibiting a higher average molecular weight than a second of two said components which second component exhibits a lower average molecular weight than said one component.

20

 20. The conduit of Claim 17, wherein said second component exhibits a calculated MI [$I_{2,16}$ according to ASTM D 1238, Condition E] of 200 to 10000dg./min.

 21. The conduit of Claim 18, wherein said one component is present in the
25 resin as a calculated weight fraction in the range of 0.20 to 0.90

 22. The conduit of Claim 18, wherein said one component is present in the resin as a calculated weight fraction in the range of 0.50 to 0.80

30 23. The conduit of Claim 18, wherein said one component is present in the resin as a calculated weight fraction in the range of 0.55 to 0.75

 24. The conduit of Claim 23 wherein the resin exhibits a density of 0.935 to 0.955 g/cc.

5

25. The conduit of Claim 23 wherein the resin exhibits a density of 0.940 to 0.950 g/cc.

26. A resin composition for the production of high performance conduits,
10 pipes, liners and coupling comprising a polyethylene resin selected from the group consisting of polymers and copolymers of ethylene and admixtures thereof, wherein the resin is characterized by FI [$I_{21.6}$, measured according to ASTM D 1238, Condition F] of 2 to 20 dg/min and a density of 0.930 to 0.960 g/cc and wherein the resin comprises at least two components, which differ from each other in average
15 molecular weight, one component of said at least two components exhibiting a higher average molecular weight than a second of said two components which second component exhibits a lower average molecular weight than said one component; wherein said second component exhibiting said lower average molecular weight exhibits a calculated MI [$I_{2.16}$, measured according to ASTM
20 D 1238, Condition E] of 200 to 10000dg./min. and wherein said resin comprises 0.20 to 0.90 weight fraction of said one component.

27. The molding composition of Claim 26, wherein the resin is made catalytically with a catalyst comprising a metallocene transition metal compound
25 wherein the resin contains a catalyst residue and thus contains up to 20 ppm of transition metal provided by said metallocene transition metal compound.

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US98/08042

A. CLASSIFICATION OF SUBJECT MATTER IPC(6) : CO8F 10/02 US CL : 428/36.91 According to International Patent Classification (IPC) or to both national classification and IPC		
B. FIELDS SEARCHED Minimum documentation searched (classification system followed by classification symbols). U.S. : 428/36.91; 525/240 Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)		
C. DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5,338,589 A [BOHM et al] 16 August 1994, col. 1, lines 23-32, col. 5, line 17.	1-27
X	US 5,539,076 A [NOWLIN et al] 23 July 1996, see abstract.	26-27
X	US 5,525,678 A [MINK et al] 11 June 1996, col. 2, lines 25-55.	26-27
A	US 4,937,299 A [EWEN et al] 26 June 1990	1-27
A	US 5,494,965 A [HARLIN et al] 27 February 1996.	1-26
<input type="checkbox"/> Further documents are listed in the continuation of Box C. <input type="checkbox"/> See patent family annex.		
* Special categories of cited documents: "A" document defining the general state of the art which is not considered to be of particular relevance "B" earlier document published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art "A" document member of the same patent family		
Date of the actual completion of the international search 01 AUGUST 1998		Date of mailing of the international search report 02 SEP 1998
Name and mailing address of the ISA/US Commissioner of Patents and Trademarks Box PCT Washington, D.C. 20231 Facsimile No. (703) 305-3230		Authorized officer CHARLES R. MOLO Telephone No. (703) 308-2351